

1. K-Theory

Derivation of Equations
a. k-Theory (Gradient Diffusion)

6 Jan 79

What is concn. in BL as fct of time & dist.?

From our derivations earlier:

$$\frac{d\bar{c}}{dt} = - \frac{\overline{w'c'}}{\bar{z}} + \dot{s} \quad \text{II.E.4.2}$$

where \dot{s} is a source^{or loss} term due to chem. reactions, radioactive decay, etc.
This describes the avg. concentration in a turbulent BL.

But $\overline{w'c'}$ is unknown (Closure Problem)

∴ Make the simplifying assumption that the flux flows down gradient,

Ex Heat flows from hot to cold
Pollutants flow from high to low concentration.

This is a very poor assumption because we are modeling the turbulent properties of the flow analogous to the molecular properties of the fluid.

Assume $\overline{w'c'} = -K \frac{\partial \bar{c}}{\partial z}$ ID.B.2.1

where $K =$ eddy diffusivity, (L^2/T)

This is known as K-Theory or Gradient Transport - bad because often there is no vertical gradient within ML

Thus

$$\frac{d\bar{c}}{dt} = \frac{\partial}{\partial z} \left(K \frac{\partial \bar{c}}{\partial z} \right) + \dot{s} \quad (\text{see 9.6 c of Dobbins})$$

If $K \neq f(z)$ then

$$\frac{d\bar{c}}{dt} = K \frac{\partial^2 \bar{c}}{\partial z^2} + \dot{S}$$

parabolic

IV. B. 2.2

b. Fickian Diffusion in 3-D

(const. K)

↳ "del squared" or Laplacian

$$\frac{d\bar{c}}{dt} = K \nabla^2 \bar{c} + \dot{S}$$

Diffusion Eq.

Heat Cond. Eq.

IV. B. 2.3

Same as 9.7 of Dobbins

Cartesian Coordinates: with no \dot{S} :

$$\frac{d\bar{c}}{dt} = K \left[\frac{\partial^2 \bar{c}}{\partial x^2} + \frac{\partial^2 \bar{c}}{\partial y^2} + \frac{\partial^2 \bar{c}}{\partial z^2} \right]$$

IV. B. 2.4

Small-eddy assumption for K -theory to work.

∴ K -theory fails during the initial spread of the puff when the eddies are larger than the puff.

a. Instantaneous ~~Puff~~ ^{Point Source} Diffusion (Puff)

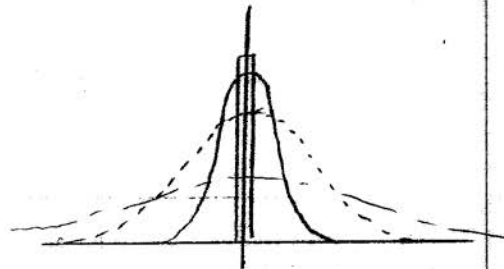
1) Diffusion of 1-D Puff

Look at 1-D problem ($c = \text{mass} / \text{dist}$)

$$\frac{d\bar{c}}{dt} = K \frac{\partial^2 \bar{c}}{\partial x^2} \quad \text{parabolic}$$

Neglect advection

$$\frac{\partial \bar{c}}{\partial t} = K \frac{\partial^2 \bar{c}}{\partial x^2}$$



Special Solution:

Problem: Find concentration as a fnt of time & dist. as diffused from an instantaneous ^{point} source of strength Q ($Q = \text{total grams}$)

Like a bomb exploding, or puff of smoke.

IC: $\bar{c} = 0$ @ $t = 0$ all x except $x = 0$

B.C. 1) $\int_{-\infty}^{\infty} \bar{c} dx = Q$ conservation of pollutants

B.C. 2) $\bar{c} \rightarrow 0$ @ $x \rightarrow \infty$

See solution in Dobbins section 7.2.1

$Q = m = \text{SS}$
 $c = \text{mass} / \text{length}$

Solution

$$\bar{c} = \frac{Q}{(4\pi Kt)^{1/2}} e^{-\left(\frac{x^2}{4Kt}\right)}$$

IV. B. 3.1

Let $\sigma(t) = \sqrt{2Kt}$ But $\sigma(t) = \sigma_r \sqrt{2T_L t}$ from Taylor at large t

$$\therefore K = \sigma_r^2 T_L$$

$$\bar{c} = \frac{Q}{\sqrt{2\pi} \sigma(t)} e^{-\frac{x^2}{2\sigma(t)^2}}$$

Answer: Proof that Gaussian is solution to Diffusion Eq.

$$c = \frac{Q}{(4\pi Kt)^{1/2}} \exp\left(-\frac{x^2}{4Kt}\right)$$

$$\begin{aligned} \frac{\partial c}{\partial t} &= \frac{Q}{(4\pi K)^{1/2}} \left[-\frac{1}{2} t^{-3/2} \cdot \exp\left(\frac{-x^2}{4Kt}\right) + t^{-1/2} \exp\left(\frac{-x^2}{4Kt}\right) \cdot \frac{x^2}{4K} t^{-2} \right] \\ &= \left\{ \frac{Q}{(4\pi Kt)^{1/2}} \exp\left(\frac{-x^2}{4Kt}\right) \cdot \frac{1}{t} \left[\frac{x^2}{4Kt} - \frac{1}{2} \right] \right\} \end{aligned}$$

$$\frac{\partial c}{\partial x} = \frac{-Q}{(4\pi Kt)^{1/2}} \exp\left(\frac{-x^2}{4Kt}\right) \cdot \frac{2x}{4Kt}$$

$$\begin{aligned} \frac{\partial^2 c}{\partial x^2} &= \frac{-Q}{(4\pi Kt)^{1/2}} \left[\exp\left(\frac{-x^2}{4Kt}\right) \cdot \frac{1}{2Kt} - \exp\left(\frac{-x^2}{4Kt}\right) \left(\frac{x}{2Kt}\right)^2 \right] \\ &= \left\{ \frac{Q}{(4\pi Kt)^{1/2}} \exp\left(\frac{-x^2}{4Kt}\right) \cdot \frac{1}{t} \left[\frac{x^2}{4Kt} - \frac{1}{2} \right] \right\} \frac{1}{K} \end{aligned}$$

$$\therefore \frac{\partial c}{\partial t} = K \frac{\partial^2 c}{\partial x^2} \quad \checkmark$$

B. From Gaussian Puff to Gaussian Plume

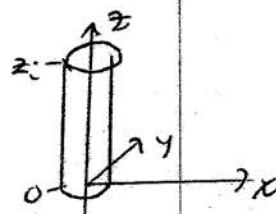
2) Similarly, for a 2-D puff:

$$c = \frac{Q}{4\pi Kt} e^{-\left(\frac{x^2+y^2}{4Kt}\right)}$$

IV.B.3.2

$Q = \text{mass}$
 $c = \text{mass/area}$
 $K_x = K_y$

Special case: cylindrical puff trapped within ML of height z_i



$$c = \frac{Q/z_i}{4\pi Kt} e^{-\left(\frac{x^2+y^2}{4Kt}\right)}$$

IV.B.3.3

$Q = \text{mass}$
 $c = \text{mass/vol}$

3) Similarly, for a 3-D puff:

$$c = \frac{Q}{(4\pi Kt)^{3/2}} e^{-\left(\frac{r^2}{4Kt}\right)}$$

IV.B.3.4

Eq 9.17 of Robbins

$Q = \text{mass}$
 $c = \text{mass/vol}$
 $r^2 = x^2 + y^2 + z^2$
 $K_x = K_y = K_z$
 (isotropic)

Special case: non-isotropic 3-D part

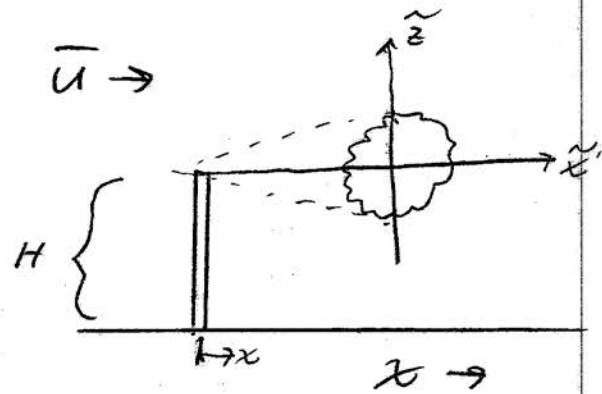
$$k_x \neq k_y \neq k_z$$

$$c = \frac{Q}{[(4\pi t)^3 k_x k_y k_z]^{1/2}} \exp\left[-\frac{1}{4t} \left(\frac{x^2}{k_x} + \frac{y^2}{k_y} + \frac{z^2}{k_z}\right)\right]$$

IV, B, 3.5

4) 3-D Puff emitted into mean wind from stack top

In a non-accelerating coordinate system moving with the puff, emitted at height H



Same as before:

$$c = \frac{Q}{[(4\pi t)^3 K_x K_y K_z]^{1/2}} \exp\left[-\frac{1}{4t} \left(\frac{\tilde{x}^2}{K_x} + \frac{y^2}{K_y} + \frac{\tilde{z}^2}{K_z}\right)\right]$$

But $\tilde{z} = z - H$

$\tilde{x} = x - \bar{u}t$ using Taylor's Hypothesis

Thus, relative to a point on the ground (below source)

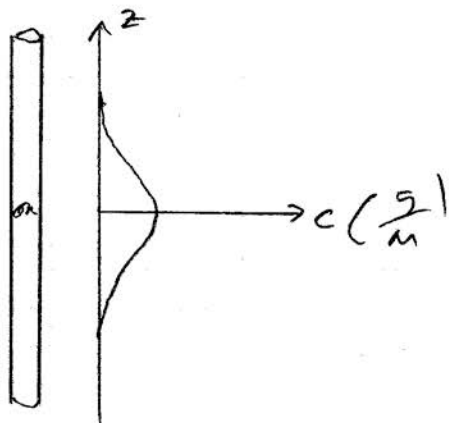
$$c = \frac{Q}{[(4\pi t)^3 K_x K_y K_z]^{1/2}} \exp\left[-\frac{1}{4t} \left(\frac{(x - \bar{u}t)^2}{K_x} + \frac{y^2}{K_y} + \frac{(z - H)^2}{K_z}\right)\right]$$

IV. 8.36

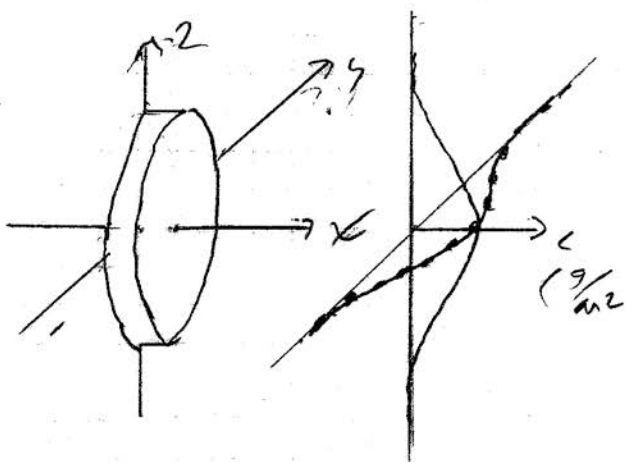
where we choose the x -direction parallel to the mean wind for simplicity.

Summary so far

1-D

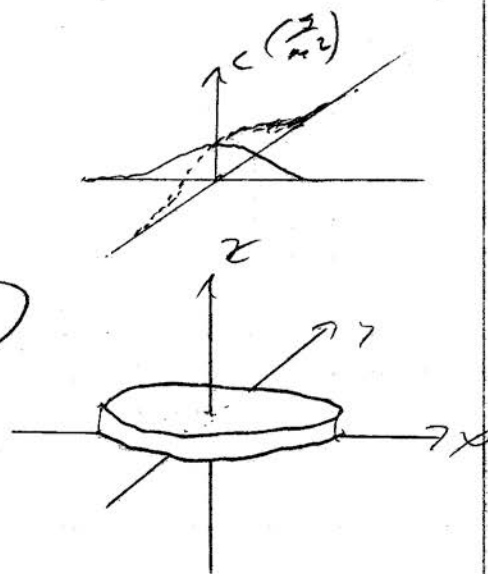


2-D disk



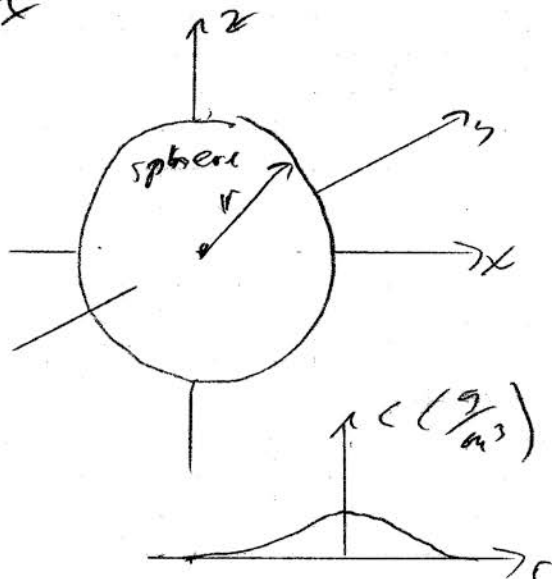
used for Gaussian plume \Rightarrow AERMOD

(OR)



used for hybrid puff/particle mode in HYSPLIT

3-D puff



Analogous to air parcel where all smoke has same mean advection as puff expands

\Rightarrow used in puff mode of HYSPLIT

AERMOD